

Solution to Problem 240B

If the boundary layer is like that of a flat plate (for which $dU/dx = 0$) then the Blasius solution applies and

$$\begin{aligned}\delta_D &= 1.72 \left(\frac{\nu x}{U} \right)^{\frac{1}{2}} \\ &= 1.72 \left(\frac{2.5 \times 10^{-6} x}{1.0} \right)^{\frac{1}{2}} m \\ &= 2.7 \times 10^{-3} x^{\frac{1}{2}} m\end{aligned}$$

The effect of this displacement thickness is to yield a volume flow rate in the tube which is the same as the volume flow rate of a *uniform* stream in a tube of radius $(R - \delta_D)$ where R is the actual radius of the tube. Therefore the velocity of the flow outside the boundary layer is not 1 m/s but U_x where

$$U\pi R^2 = U_x\pi (R - \delta_D)^2$$

At $x = 200 \text{ m}$, where $\delta_D = 0.038 \text{ m}$ this yields

$$U_x = \frac{U}{(1 - \delta_D/R)^2} = 1.39 \text{ m/s}$$

Since Bernoulli's equation applies outside the boundary layer the pressure at $x = 200 \text{ m}$ is related to the pressure at the inlet ($x = 0 \text{ m}$) by

$$\begin{aligned}p_{x=200 \text{ m}} - p_{x=0 \text{ m}} &= \frac{1}{2}\rho [U^2 - U_x^2] \\ &= -0.57 \text{ Pa}\end{aligned}$$

where $\rho = 1.2 \text{ kg/m}^3$.

In order to proceed to a more accurate solution that takes this pressure and velocity gradient into account, one might approximately estimate the value of the Falkner-Skan m from

$$m = \frac{x}{U} \frac{dU}{dx} \approx \frac{U_{x=200 \text{ m}}}{U} - 1 = 0.39$$

and then use the Falkner-Skan solution for this value of m instead of the Blasius solution to evaluate the displacement thickness.